

**TOTAL CHROMIUM EMISSIONS  
TESTING REPORT**

**Performed for:**

**CENTURY PLATING COMPANY, INC.  
CHICAGO, ILLINOIS**

**Performed By:**

**RMC Environmental, Inc.  
Project Number: 98-015-311**


**RMC Environmental, Inc.**  
**PO Box 1008**  
**Elgin, Illinois 60121-1008**

**800-532-3391 Voice**  
**847-669-5389 Fax**

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29 September 1998

I, Rachel M. Chleborowicz, certify that the Chromium Emissions Testing conducted on the decorative plating scrubber installed at the Century Plating Company, Inc. facility in Chicago, Illinois, was conducted under my supervision. All of the results obtained during this testing are authentic and accurate.



**Rachel Chleborowicz**  
**Project Manager**

**Prepared by:**

**CENTURY PLATING, INC.  
CHICAGO, ILLINOIS**

**Submitted By:**

**RMC Environmental, Inc.  
11311-B Douglas Street  
Huntley, Illinois 60142**

**RMCEI Reference Number: 98-015-311**

**September 1, 1998**

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TEST REPORT  
For  
Century Plating, Inc.  
Chicago, Illinois**

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## 1.0 PROJECT SUMMARY

### 1.1 Source Information

Plant Name and Address: Century Plating Company, Inc.  
2939 North Oakley Avenue  
Chicago, Illinois 60618

Units Tested: Primary Decorative chrome tank scrubber.

### 1.2 Testing Firm Information

Firm Name and Address: RMC Environmental, Inc.  
11311-B Douglas Street  
Huntley, Illinois 60142

Firm Contact: Rachel M. Chleborowicz - Project Manager

Telephone Number: 800-532-3391 Voice  
847-669-5389 Fax

### 1.3 Test Information

Test Requested By: Century Plating Company, Inc.

Firm Contact: Mr. Victor LaPorta

Telephone Number: 773-477-1620 Phone  
773-477-1823 Fax

Test Objective: Conduct total chrome, moisture and flow rate testing on plating tanks in accordance with the MACT regulations and EPA Method 306 (40 CFR 63, Appendix A).

Test Methods: EPA Methods 1, 2, 3, 4 and 306

Test Date: September 1, 1998

Test Coordinators: Mr. Victor LaPorta

Test Personnel: Rachel Chleborowicz - Project Manager  
Chris McDermid - Environmental Technician

## 2.0 SUMMARY OF RESULTS

The results of the emissions testing performed on the large chrome tank stack are presented in **Table 2-1**. Detailed results of all of the testing completed on this location are located in **Appendix A**. The field data and the analytical results are presented in **Appendix B** and **C**, respectively. Calibration sheets and equipment performance checks are presented in **Appendix D**, along with the chain of custody and QA/QC supporting documentation from the analytical laboratory.

A cyclonic flow check was performed at the sampling location to determine the existence of abnormal flow. The observed average yaw angle for the secondary unit location was 9.5°. Section 2.5 of EPA Method 1 indicates that a sampling location with an average yaw angle of  $\leq 20^\circ$  is acceptable. As indicated by the average of the three test runs, the concentrations of the chromium emissions were below the MACT regulation standards of and 0.030 mg/DSCM for composite mesh pad scrubber systems on decorative chrome plating tanks.

**TABLE 2-1**  
**SUMMARY OF TOTAL CHROMIUM RESULTS**

Century Plating Company, Inc.  
September 1, 1998

Location	Test Parameter	Result	Specification
Secondary Plating Tank Stack	mg/DSCM Flow rate DSCFM	0.005 8,045	$\leq 0.030$ mg/DSCM for existing large sources

### 3.0 TEST PROCEDURES AND EMISSIONS DETERMINATIONS

The sampling and analytical requirements for this program include the determination of total chrome,  $O_2/CO_2$ , moisture and volumetric flowrates from the stack effluent. The plating process was operated at 100% capacity. Figure 3-1 illustrates the sampling system used for the total chrome testing. The specific equipment and procedures that were used are detailed below.

#### 3.1 Test Procedures

Total chrome compliance testing was completed on the exhaust stacks from the chrome plating tanks. The compliance testing consisted of three two-hour test runs utilizing EPA Methods 1, 2, 3B (40 CFR 60, Appendix A) and 306 (40 CFR 63, Appendix A).

The number and location of the sampling points were determined according to the procedures outlined in EPA Method 1. The exhaust stack cross section was divided into 24 equal areas with 12 sampling points on each of two axes. A cyclonic flow check was performed at the sampling location to determine the flow angles at each point. An S-type pitot, oil manometer, and an angle finder were used for these determinations. At each point, the Pitot was positioned at a right angle to the flow, the pitot was then rotated until a null reading was obtained. The angles of rotation were then noted.

The flue gas velocity and volumetric flow rates were determined according to EPA Method 2. Velocity head measurements ( $\Delta P$ ) were made using an S-type Pitot tube conforming to the geometric specifications indicated in Method 2 and each Pitot has been assigned a coefficient of 0.84. The differential pressures were measured using an oil manometer of the appropriate range. Flue gas temperatures were obtained with chromel-alumel thermocouples equipped with a digital readout.

The composition of the flue gas was determined utilizing the procedures outlined in Method 3B. The percent moisture content of the flue gas was obtained from the amount of moisture collected in the Method 306 sampling train. Analysis for carbon dioxide and oxygen were performed using a Fyrite analyzer and the analytical results were used in the calculation of flue gas composition and molecular weight.

#### 3.2 Emissions Determinations

The total chrome samples were drawn isokinetically from the source using an EPA method 306 sampling train. The sampling train consisted of a glass nozzle and probe liner, an attached Type S Pitot tube, four glass impinger chilled and a metering console. No filter is used for this method.

The first impinger is left empty, the second and third impingers contain 100 ml of 0.1 N sodium hydroxide (NaOH) in place of water, and the fourth impinger contains 200g of preweighed silica gel for moisture removal. Each of the twenty-four points were sampled for 5 minutes resulting in a net run time of 120 minutes.

After sampling, the reagents were returned to their original container, weighed, the weights recorded on the label and the liquid level marked. The silica gel was returned to the original container, weighed and the weight recorded on the label. The volume of water vapor condensed in the impingers and the volume of water collected in the silica gel

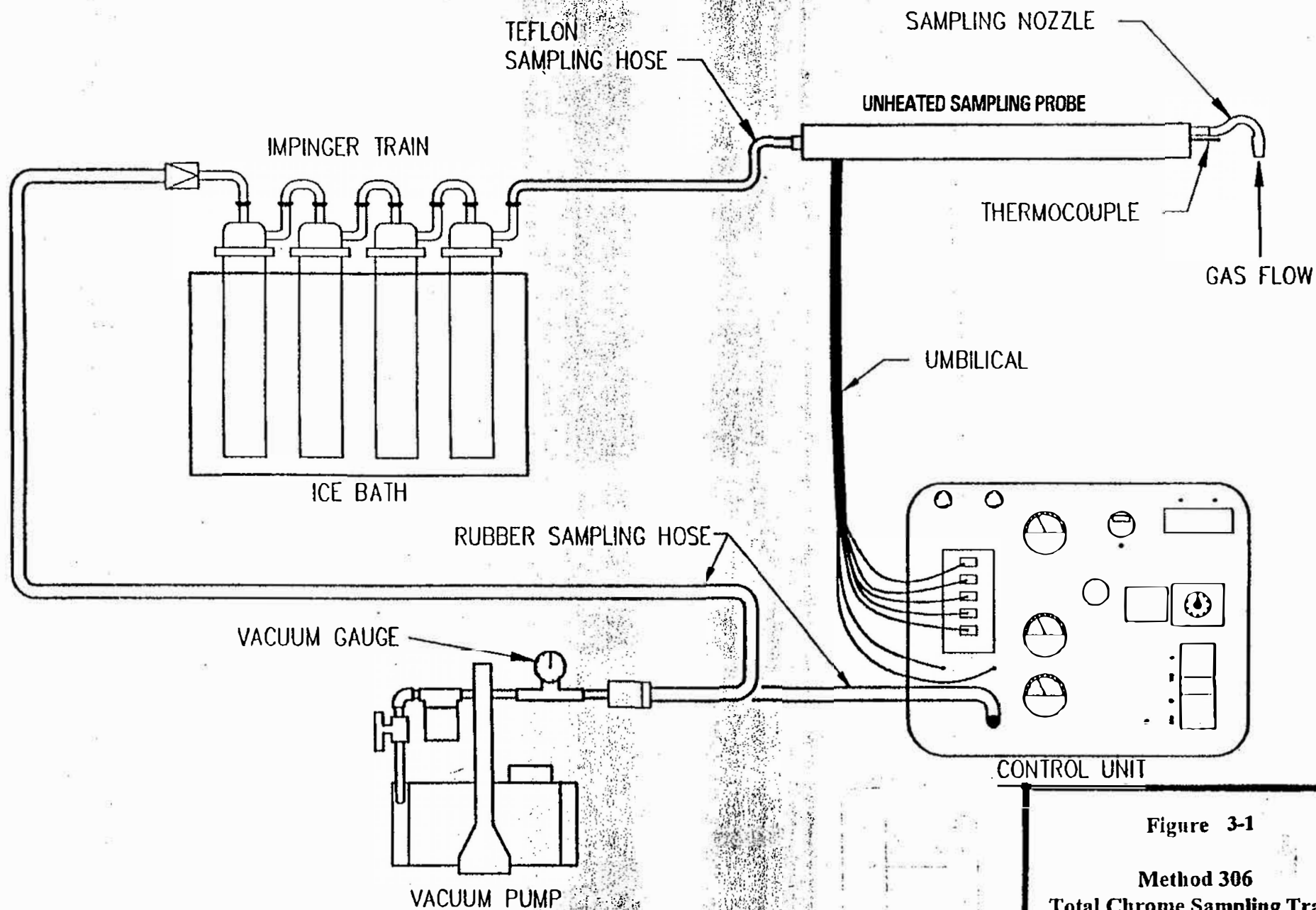


Figure 3-1

**Method 306**  
**Total Chrome Sampling Train**



were summed and entered into the moisture content calculations. All sampling components exposed to the effluent were rinsed three time with NaOH and the rinses were added to the reagent containers.

The combined samples and rinses were analyzed for total chrome using ion chromatography (IC) coupled with a post-column reactor (PCR).

## **Appendix A - Reference Measurement Data With Emission Rate Calculations**

**RMC Environmental, Inc.**  
**Emissions Testing & Consulting**

Plant: Century Plating  
Project #: 98-015-311  
Location: Unit 1 - Mesh Pad System

Date: 09/16/98

Sample Identification  
Test Date

1-M306-1 1-M306-2 1-M306-3  
09/01/98 09/01/98 09/01/98

Start	810	1030	1240
Finish	1015	1235	1445
Total	120	120	120

Cp	Pitot Coefficient	(CF)	0.84	0.84	0.84
A	Area of stack	sq. inches	530.93	530.93	530.93
Pbar	Barometric Pressure	(in HG)	30.12	30.12	30.18
Wm	Volume of Condensate	(mg)	47.6	47.1	50.4
Ts	Temperature of Effluent	(F)	93.1	93.3	93.9
Pavg	Average Delta P		0.460	0.455	0.450
Pg	Static Pressure	(in H2O)	-0.25	-0.28	-0.24
DH	Delta H, Orifice pressure differential	(in H2O)	1.82	1.83	1.81
Tm	Meterbox Temperature	(F)	80.6	89.5	91.1
Vm	Volume of sample metered	(CF)	90.14	90.693	90.966
Y	Meter correction factor		0.9999	0.9999	0.9999
Dn	Nozzle Diameter	(in)	0.25	0.25	0.25
CO2	Percent Carbon Dioxide	(%)	0.10	0.10	0.10
O2	Percent Oxygen	(%)	20.90	20.80	20.90
CO	Percent Carbon Monoxide	(%)	0	0	0
N2	Percent Nitrogen	(%)	79.00	79.10	79.00
Ms	Molecular Weight (wet)	(lb/lb-m)	28.59	28.58	28.57

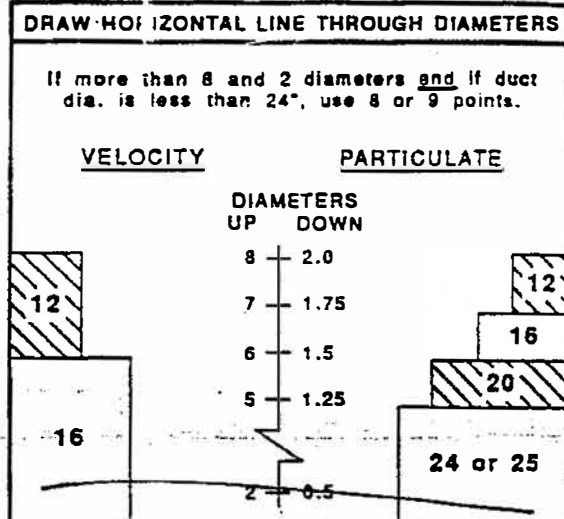
**Laboratory Results**

	Total Chrome	(mg)	5.80E-03	5.10E-03	2.90E-02
Ps	Absolute pressure of Flue Gas	(in HG)	30.10	30.10	30.16
Vwstd	Volume of Water Vapor	(SCF)	2.24	2.22	2.38
Vmstd	Volume of Metered Gas	(DSCF)	88.978	88.075	88.255
M	Moisture	(%)	2.46	2.46	2.62
Vs	Velocity	(FPS)	39.06	38.85	38.61
Qaw	Volumetric Flow	(ACFM)	8,641	8,594	8,541
Qsd	Volumetric Flow	(DSCF)	8,095	8,047	7,993
	Chromium Concentration	(mg/DSCM)	0.002	0.002	0.012
	Chromium Concentration	(lb/Hr)	6.98E-05	6.16E-05	3.47E-04
I	Isokenetic	(%)	99.07	98.65	99.52

**Appendix B - Field Data Sheets For Total Chrome**

# Sampling and Velocity Traverse Point Determination EPA Method 1

PLANT NAME <u>CENTURY PLATING</u>	
CITY, STATE <u>Chicago IL</u>	
SAMPLING LOCATION <u>DEC. PLATING TANK Scribe</u>	
NO. OF PORTS AVAILABLE	<u>2</u>
NO. OF PORTS USED	<u>2</u>
PORT INSIDE DIAMETER	<u>3"</u>
DISTANCE FROM FAR WALL TO OUTSIDE OF PORT	<u>36.75</u>
NIPPLE LENGTH AND/OR WALL THICKNESS	<u>0.75</u>
DEPTH OF STACK OR DUCT	<u>36</u>
STACK OR DUCT WIDTH (IF RECTANGULAR)	<u>-</u>
EQUIVALENT DIAMETER: $D_e = \frac{2 \times \text{DEPTH} \times \text{WIDTH}}{\text{DEPTH} + \text{WIDTH}} = \frac{2 ( \quad ) ( \quad )}{( \quad ) + ( \quad )} = \underline{\hspace{2cm}}$	
DISTANCE FROM PORTS TO FLOW DISTURBANCES	<div style="display: flex; justify-content: space-between;"> <span>UPSTREAM</span> <span>DOWNSTREAM</span> </div>
DIAMETERS	
STACK/DUCT AREA = <u>                    </u> = <u>1017.9</u> IN <sup>2</sup>	



**LOCATION OF POINTS IN CIRCULAR STACKS OR DUCTS**

	4	6	8	10	12	14	16	18	20	22	24
1	6.7	4.4	3.2	2.8	2.1	1.8	1.6	1.4	1.3	1.1	1.1
2	25.0	14.6	10.5	8.2	6.7	5.7	4.9	4.4	3.9	3.5	3.2
3	75.0	29.8	19.4	14.6	11.8	9.9	8.5	7.5	6.7	6.0	5.5
4	93.3	70.4	52.3	42.6	37.7	34.2	31.2	28.3	25.9	23.9	22.2
5	95.6	85.8	77.4	70.4	64.4	59.4	55.4	52.3	49.4	46.8	44.4
6	97.9	90.1	83.1	76.4	70.4	64.4	59.4	55.4	52.3	49.4	46.8
7	99.1	93.3	87.5	81.2	75.0	68.8	62.5	56.2	50.0	43.8	37.5
8	100.0	95.1	90.1	85.1	80.1	75.0	69.9	64.8	59.7	54.6	49.4
9	100.0	96.1	91.1	86.1	81.1	76.1	71.1	66.1	61.1	56.1	51.1
10	100.0	97.4	92.4	87.4	82.4	77.4	72.4	67.4	62.4	57.4	52.4
11	100.0	98.2	93.2	88.2	83.2	78.2	73.2	68.2	63.2	58.2	53.2
12	100.0	98.9	93.9	88.9	83.9	78.9	73.9	68.9	63.9	58.9	53.9
13	100.0	99.1	94.1	89.1	84.1	79.1	74.1	69.1	64.1	59.1	54.1
14	100.0	99.1	94.1	89.1	84.1	79.1	74.1	69.1	64.1	59.1	54.1
15	100.0	99.1	94.1	89.1	84.1	79.1	74.1	69.1	64.1	59.1	54.1
16	100.0	99.1	94.1	89.1	84.1	79.1	74.1	69.1	64.1	59.1	54.1
17	100.0	99.1	94.1	89.1	84.1	79.1	74.1	69.1	64.1	59.1	54.1
18	100.0	99.1	94.1	89.1	84.1	79.1	74.1	69.1	64.1	59.1	54.1
19	100.0	99.1	94.1	89.1	84.1	79.1	74.1	69.1	64.1	59.1	54.1
20	100.0	99.1	94.1	89.1	84.1	79.1	74.1	69.1	64.1	59.1	54.1
21	100.0	99.1	94.1	89.1	84.1	79.1	74.1	69.1	64.1	59.1	54.1
22	100.0	99.1	94.1	89.1	84.1	79.1	74.1	69.1	64.1	59.1	54.1
23	100.0	99.1	94.1	89.1	84.1	79.1	74.1	69.1	64.1	59.1	54.1
24	100.0	99.1	94.1	89.1	84.1	79.1	74.1	69.1	64.1	59.1	54.1

**LOCATION OF POINTS IN RECTANGULAR STACKS OR DUCTS**

	2	3	4	5	6	7	8	9	10	11	12
1	25.0	16.7	12.5	10.0	8.3	7.1	6.3	5.6	5.0	4.5	4.2
2	75.0	50.0	37.5	30.0	25.0	21.4	18.8	16.7	15.0	13.6	12.5
3	93.3	62.5	50.0	41.7	35.7	31.3	27.8	25.0	22.7	20.8	19.4
4	95.6	64.4	52.3	44.4	38.3	33.9	30.4	27.9	25.9	23.9	22.2
5	97.9	66.1	54.1	46.1	40.1	35.7	32.3	29.8	27.4	25.4	23.9
6	99.1	67.4	55.4	47.4	41.4	37.0	33.6	31.2	29.2	27.2	25.7
7	100.0	68.2	56.2	48.2	42.2	37.8	34.4	32.0	30.0	28.0	26.5
8	100.0	68.9	56.9	48.9	42.9	38.5	35.1	32.7	30.7	28.7	27.2
9	100.0	69.1	57.1	49.1	43.1	38.7	35.3	32.9	30.9	28.9	27.4
10	100.0	69.1	57.1	49.1	43.1	38.7	35.3	32.9	30.9	28.9	27.4
11	100.0	69.1	57.1	49.1	43.1	38.7	35.3	32.9	30.9	28.9	27.4
12	100.0	69.1	57.1	49.1	43.1	38.7	35.3	32.9	30.9	28.9	27.4

POINT	% OF DUCT DEPTH	DISTANCE FROM INSIDE WALL	DISTANCE FROM OUTSIDE OF PORT
1	2.1	0.76	1.5
2	6.7	2.4	3.2
3	11.8	4.2	5.0
4	17.7	6.4	7.2
5	25.0	9.0	9.8
6	35.6	12.8	13.6
7	64.4	23.2	24.0
8	75.0	27.0	27.8
9	82.3	29.6	30.4
10	88.2	31.8	32.6
11	93.3	33.6	34.4
12	97.9	35.2	36.0
13			
14			
15			
16			
17			
18			
19			
20			
21			
22			
23			
24			

## Page 1 of 1

[illegible]

See page 2 for cyclonic flow check criteria.

CLIENT

PLANT

CITY/STATE

SAMPLING LOC.

BAROMETRIC PRESSURE, IN. HG.

LEAK V, VACUUM IN. HG.

LEAK RATE, CFM

RUN NO. 1-306-01

JOB NO. 98-015-211 DATE 1 Sept 98

TIME START 810

TIME FINISH 1015

TEST PERSONNEL RWC/CMD

POSTTEST POS PRESS LEAK / OK7

\* CONDUCT POSTTEST POSITIVE PRESSURE LEAK CHECK FOLLOWING THE LAST RUN PER LOCATION. FOR OTHER RUNS, ENTER "N/A".

EQUIPMENT CHECKS		EQUIPMENT I.D. NUMBERS		LEAK CHECKS	
<input checked="" type="checkbox"/> PITOT, PRETEST	REAGENT BOX	METER BOX 71-22	Y 0.9999	B	B
<input type="checkbox"/> PITOT, POSTTEST	PITOT M-2-1	Cp 0.81	NOZ'L N-250 DIA. 0.250	E	E
<input checked="" type="checkbox"/> NOZZLE, PRE/POST	TC READOUT	TC PROBE	UMBILICAL	B	B
<input checked="" type="checkbox"/> TC 30 °F PRE	SAMPL'G BOX	ORSAT PUMP	TEDLAR BAG	E	E
<input checked="" type="checkbox"/> TC 70 °F POST					
<input checked="" type="checkbox"/> ORSAT SYSTEM	MONOGRAPH DATA				
FILTER/XAD	TARE WT.	DELTA-H2	METER TEMP.	Fyrites, %	Yca
N.O.H.	200.6	1.7970	80	0.2	0.995
	229	EST. XH2O	2	CO2	0.9
	29	"C" FACTOR	1.022	5% OF CAL'D Y7	
Silicad.	200	STACK TEMP.	93	(Y) (N)	
	218.6	REF DELTA-P	0.463		
		"K" FACTOR	3.974		

38.91 ft/sec.

L I N E	SAMPLE POINT	CLOCK TIME, MINUTES	DRY GAS METER READING, CUBIC FEET	PITOT READING, IN. H2O	GAS METER TEMP., °F	STACK TEMP., °F	ORIFICE SETTING, IN. H2O		GAUGE VACUUM, IN. HG	GAS TEMPERATURES, °F			✓
							ACTUAL	IDEAL		FILTER	IMPING. EXIT	PROBE OR COND EXIT**	
1	A-1	0	624.632	0.46	72	92	1.8	1.8	4		54		✓
2	2	5	628.36	0.49	73	93	1.91	1.91	4		54		
3	3	10	632.19	0.48	74	93	1.88	1.88	4		55		
4	4	15	635.92	0.47	74	94	1.84	1.84	4		54		
5	5	20	639.75	0.47	75	94	1.84	1.84	4		56		
6	6	25	643.58	0.45	76	95	1.77	1.77	4		56		
7	7	30	647.41	0.48	77	95	1.87	1.87	4		57		
8	8	35	651.24	0.46	78	95	1.81	1.81	4		57		
9	9	40	655.07	0.45	79	95	1.78	1.78	4		57		
10	10	45	658.90	0.43	80	93	1.7	1.7	4		58		
11	11	50	662.73	0.47	81	93	1.86	1.86	4		58		
12	12	55	666.56	0.46	82	93	1.83	1.83	4		58		
13	B-1	60	669.39	0.43	82	93	1.91	1.91	4		57		
14	2	65	673.22	0.45	82	93	1.79	1.79	4		57		
15	3	70	676.05	0.45	83	93	1.79	1.79	4		57		
16	4	75	679.88	0.44	83	93	1.75	1.75	4		58		
17	5	80	683.71	0.43	84	93	1.72	1.72	4		58		
18	6	85	687.54	0.46	84	93	1.84	1.84	4		58		
19	7	90	691.37	0.46	85	93	1.84	1.84	4		58		
20	8	95	695.20	0.47	85	93	1.88	1.88	4		58		
21	9	100	699.03	0.46	86	93	1.84	1.84	4		59		
22	10	105	702.86	0.48	86	93	1.92	1.92	4		59		
23	11	110	706.69	0.48	87	93	1.92	1.92	4		60		
24	12	115	710.52	0.47	87	94	1.88	1.88	4		60		
25	END	120	714.35										✓

FINAL

\* FILTER EXIT for NJ Method 1. FILTER BOX for all others.

\*\* PROBE EXIT &amp; / (probe &amp; filter heat off) apply to NJ Method 1. COND. EXIT applies if sampling train has a condenser.

120 90.140 0.4603 80.6 93.1 1.8246  
 Min. (e) Vm ( $\sqrt{\Delta P}$ )<sup>2</sup> cm ts ΔH



# SAMPLING DATA - METHOD(S)

306

CLIENT Cenova Plating RUN NO. L-306-02  
 PLANT Chicago, IL JOB NO. 99-015-311 DATE 1 Sept 98  
 CITY/STATE Chicago, IL TIME START 1030  
 SAMPLING LOC. Unit 1 - Decorative Plating TIME FINISH 1235  
 BAROMETRIC PRESSURE, IN. HG 30.12 STATIC PRESSURE, IN. H<sub>2</sub>O -0.28  
 LEAK 1, VACUUM IN. HG 10 5 TEST PERSONNEL RMC/CMC  
 LEAK RATE, CFM 0.001 POSTTEST POS PRESS LEAK 1 OK?

\* CONDUCT POSTTEST POSITIVE PRESSURE LEAK CHECK FOLLOWING THE LAST RUN PER LOCATION. FOR OTHER RUNS, ENTER "N/A".

EQUIPMENT CHECKS		EQUIPMENT I.D. NUMBERS		LEAK CHECKS	
<input checked="" type="checkbox"/> PITOT, PRETEST	REAGENT BOX <u>N/A</u>	METER BOX <u>71-22</u>	Y <u>0.9999</u>	B <u></u>	B <u></u>
<input checked="" type="checkbox"/> PITOT, POSTTEST	PITOT <u>M-2-1</u>	CP <u>0.84</u>	NOZ'L <u>N-25</u>	DIA. <u>0.250</u>	E <u></u>
<input checked="" type="checkbox"/> NOZZLE, PRE/POST	TC READOUT <u></u>	TC PROBE <u></u>	UMBILICAL <u></u>	B <u></u>	B <u></u>
<input checked="" type="checkbox"/> TC 78 °F PRE	SAMPL'G BOX <u></u>	ORSAT PUMP <u></u>	TEDLAR BAG <u></u>	E <u></u>	E <u></u>
<input checked="" type="checkbox"/> TC 78 °F POST					
<input checked="" type="checkbox"/> ORSAT SYSTEM	NOMOGRAPH DATA				
	DELTA-H <sub>2</sub> O <u>1.797</u>			B <u></u>	B <u></u>
FILTER/XAD	TARE WT.	METER TEMP. <u>90</u>		E <u></u>	E <u></u>
<u>NaOH</u>	<u>200.6</u>	EST. XH <sub>2</sub> O <u>2</u>			
	<u>232</u>	"K" FACTOR <u>0.022</u>	<u>1.041</u>		
		STACK TEMP. <u>83</u>	<u>93</u>		
<u>5/16 in.</u>	<u>200g</u>	REF DELTA-P <u>0.463</u>	<u>0.455</u>		
	<u>215.1</u>	"K" FACTOR <u>3.974</u>	<u>4.048</u>		
				Fyrites, % <u>0.208</u>	Ics <u>0.999</u>
				CO <sub>2</sub> <u>0.9</u>	% OF CAL'D. Y? <u>(Y) (N)</u>

38.69 <sup>cm</sup>/sec

LINE	SAMPLE POINT	CLOCK TIME, MINUTES	DRY GAS METER READING, CUBIC FEET	PITOT READING, IN. H <sub>2</sub> O	GAS METER TEMP., °F	STACK TEMP., °F	ORIFICE SETTING, IN. H <sub>2</sub> O		GAUGE VACUUM, IN. HG	GAS TEMPERATURES, °F			✓
							ACTUAL	IDEAL		FILTER *	IMPING. EXIT	PROBE OR COND. EXIT**	
1	A-1	0	719.915	0.45	87	93	1.81	1.91	4	N/A	60	N/A	✓
2	2	5	719.695	0.44	87	93	1.77	1.77	4		51		
3	3	10	722.32	0.43	88	93	1.73	1.73	4		51		
4	4	15	726.01	0.46	88	93	1.85	1.85	4		53		
5	5	20	729.79	0.47	89	93	1.89	1.89	4		54		
6	6	25	733.67	0.46	89	93	1.85	1.85	4		54		
7	7	30	737.55	0.45	89	93	1.81	1.81	4		54		
8	8	35	741.43	0.44	89	93	1.77	1.77	4		54		
9	9	40	745.31	0.43	89	93	1.73	1.73	4		54		
10	10	45	749.19	0.44	89	93	1.77	1.77	4		54		
11	11	50	752.67	0.44	89	93	1.77	1.77	4		54		
12	12	55	756.35	0.43	90	94	1.73	1.73	3		54		
13	B-1	60	760.004	0.46	89	93	1.85	1.85	4		54		
14	2	65	764.05	0.45	89	94	1.81	1.81	4		58		
15	3	70	767.84	0.47	89	93	1.89	1.89	4		58		
16	4	75	771.66	0.47	89	93	1.89	1.89	4		58		
17	5	80	775.55	0.48	90	94	1.93	1.93	4		58		
18	6	85	779.37	0.48	90	94	1.93	1.93	4		57		
19	7	90	783.25	0.47	90	94	1.89	1.89	4		57		
20	8	95	787.06	0.47	90	94	1.89	1.89	4		58		
21	7	100	790.84	0.43	91	94	1.81	1.81	4		58		
22	10	105	794.59	0.43	91	94	1.73	1.73	3		58		
23	11	110	798.26	0.44	91	94	1.77	1.77	3		59		
24	12	115	801.99	0.42	91	94	1.69	1.69	3		59		✓
25	END	120	805.608							✓		✓	

FINAL

\* FILTER EXIT for NJ Method 1. FILTER BOX for all others.

\*\* PROBE EXIT & / (probe & filter heat off) apply to NJ Method 1. COND. EXIT applies if sampling train has a condenser.

120 90.693 0.455 89.5 93.3 1.831  
 Min. (B) Vm ( $\sqrt{\Delta P}$ )<sup>2</sup> tm ts ΔH

% = 100.3

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CLIENT Century Planning Co., Inc. RUN NO. 1-306-03  
 PLANT Chicago, IL JOB NO. 98-015-311 DATE 1 Sept 77  
 CITY/STATE Chicago, IL TIME START 1240  
 SAMPLING LOC. Unit 11 TIME FINISH 1435  
 BAROMETRIC PRESSURE, IN. HG 30.18 STATIC PRESSURE, IN. H<sub>2</sub>O -0.24  
 LEAK 1, VACUUM IN. HG 0 5" TEST PERSONNEL Rafael  
 LEAK RATE, CFM 0.000 0.003 POSTTEST POS PRESS LEAK 1 OK?

• CONDUCT POSTTEST POSITIVE PRESSURE LEAK CHECK FOLLOWING THE LAST RUN PER LOCATION. FOR OTHER RUNS, ENTER "N/A".

EQUIPMENT CHECKS		EQUIPMENT I.D. NUMBERS		LEAK CHECKS	
<input checked="" type="checkbox"/> PITOT, PRETEST	REAGENT BOX <u>N/A</u>	METER BOX <u>71.22</u>	Y <u>0.9999</u>	B <u></u>	B <u></u>
<input checked="" type="checkbox"/> PITOT, POSTTEST	PITOT <u>M-2-1</u>	NOZ'L <u>N-250</u>	DIA. <u>0.250</u>	E <u></u>	E <u></u>
<input checked="" type="checkbox"/> NOZZLE, PRE/POST	TC READOUT <u></u>	TC PROBE <u></u>	UMBILICAL <u></u>	B <u></u>	B <u></u>
<input checked="" type="checkbox"/> TC <u>81</u> °F PRE	SAMPL'G BOX <u></u>	ORSAT PUMP <u></u>	TEDLAR BAG <u></u>	E <u></u>	E <u></u>
<input checked="" type="checkbox"/> TC <u>81</u> °F POST				B <u></u>	B <u></u>
<input checked="" type="checkbox"/> ORSAT SYSTEM				E <u></u>	E <u></u>
		MONOGRAPH DATA			
DELTA-HG <u>1.797</u>					
FILTER/XAD	TARE WT.	METER TEMP.			
<u>N/A</u>	<u>200.6</u>	EST. H <sub>2</sub> O	<u>2</u>		
	<u>234</u>	"C" FACTOR	<u>1.041</u>		
		STACK TEMP.	<u>93</u>		
<u>Silad</u>	<u>200.4</u>	REF DELTA-P	<u>0.463</u>		
	<u>216.4</u>	"K" FACTOR	<u>3.974</u>		
				Fyrites, %	IGA
				<u>O<sub>2</sub> 20.9</u>	<u>0.993</u>
				<u>CO<sub>2</sub> 0.1</u>	% OF CAL'D Y7
					(Y) <u></u> (N) <u></u>

L I N E	SAMPLE POINT	CLOCK TIME, MINUTES	DRY GAS METER READING, CUBIC FEET	PITOT READING, IN. H <sub>2</sub> O	GAS METER TEMP., °F	STACK TEMP., °F	ORIFICE SETTING, IN. H <sub>2</sub> O		GAUGE VACUUM, IN. HG	GAS TEMPERATURES, °F		
							ACTUAL	IDEAL		FILTER	IMPING. EXIT	PROBE OR COND EXIT**
1	A-1	0	805.961	0.43	90	94	1.83	1.83	4	N/A	54	N/A
2	2	5	809.69	0.45	89	94	1.81	1.81	4		53	
3	3	10	813.43	0.44	89	94	1.77	1.77	4		53	
4	4	15	817.14	0.46	90	94	1.86	1.86	4		53	
5	5	20	820.91	0.47	90	93	1.89	1.89	4		53	
6	6	25	824.76	0.48	90	93	1.94	1.94	4		53	
7	7	30	828.64	0.48	91	93	1.94	1.94	4		54	
8	8	35	832.52	0.45	91	94	1.81	1.81	4		54	
9	9	40	836.21	0.46	91	94	1.85	1.85	4		54	
10	10	45	840.01	0.43	92	94	1.74	1.74	4		54	
11	11	50	843.75	0.42	92	94	1.70	1.70	4		55	
12	12	55	847.44	0.39	92	95	1.57	1.57	4		55	
13	B-1	60	851.004	0.40	92	95	1.61	1.61	4		56	
14	2	65	854.66	0.43	92	95	1.73	1.73	4		56	
15	3	70	858.34	0.44	92	95	1.77	1.77	4		56	
16	4	75	862.15	0.44	92	95	1.77	1.77	4		56	
17	5	80	865.91	0.47	91	94	1.90	1.90	4		57	
18	6	85	869.79	0.47	91	94	1.89	1.89	4		57	
19	7	90	873.64	0.45	91	94	1.81	1.81	4		58	
20	9	95	877.49	0.46	92	94	1.86	1.86	4		58	
21	1	100	881.32	0.48	92	93	1.94	1.94	4		58	
22	10	105	885.24	0.48	91	93	1.94	1.94	4		59	
23	11	110	889.14	0.47	91	93	1.89	1.89	4		59	
24	12	115	893.01	0.45	91	94	1.81	1.81	4		60	
25	END	120	896.927									

FINAL

\* FILTER EXIT for NJ Method 1. FILTER BOX for 11 others.

\*\* PROBE EXIT &amp; / (probe &amp; filter heat off) apply to NJ Method 1. COND. EXIT applies if sampling train has a condenser.

120. 90.966 0.4497 91.1 93.9 1.814  
 Min. (B) Vm (1/ΔP)<sup>2</sup> tm ts ΔH

% 100.9  
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# MOISTURE ANALYTICAL RESULTS

Client CENTURY PLATING

Plant Name \_\_\_\_\_

Job No. 98-015-311

City/State Chicago, IL

Sampling Loc. Dec. Plating tank

Run Number	1-306-01	1-306-02	1-306-03
Sampling Date	<u>9/1/98</u>	<u>9/1/98</u>	<u>9/1/98</u>
Analysis Date	<u>"</u>	<u>"</u>	<u>"</u>
Analyst	<u>Rue</u>	<u>Rue</u>	<u>Rue</u>

<u>Reagent 1 (0.1N NaOH)</u>			
Final Weight, g	<u>229</u>	<u>232</u>	<u>234</u>
Tared Weight, g	<u>200</u>	<u>200</u>	<u>200</u>
Water Catch, g	<u>29</u>	<u>32</u>	<u>34</u>
<u>Reagent 2 ( )</u>			
Final Weight, g			
Tared Weight, g			
Water Catch, g			
<u>Reagent 3 ( )</u>			
Final Weight, g			
Tared Weight, g			
Water Catch, g			
CONDENSED WATER, g	<u>29</u>	<u>32</u>	<u>34</u>
<u>Silica Gel</u>			
Final Weight, g	<u>218.6</u>	<u>215.1</u>	<u>216.4</u>
Tared Weight, g	<u>200</u>	<u>200</u>	<u>200</u>
ADSORBED WATER, g	<u>18.6</u>	<u>15.1</u>	<u>16.4</u>
TOTAL WATER COLLECTED, g	<u>47.6</u>	<u>47.1</u>	<u>50.4</u>

Balance No. Rue-015 Type ☒ Triple Beam ☐ Electronic ☒ Reagent Box No. \_\_\_\_\_

Balance located in stable, draft-free area ☒ Yes ☐ No (If "No", explain below.)

Comments \_\_\_\_\_